

1. Introduction

Pharmaceutical manufacturing relies heavily on tradition batch stirred tank crystallisers (STC's) for the production of crystalline active pharmaceutical ingredients (APIs). Despite the successful implementation of batch manufacturing of APIs, achieving robust process control of STC's can be limited and there is considerable interest in exploiting the opportunities for enhanced control that continuous processing technologies offer. One such technology, the continuous oscillatory baffled crystalliser (COBC), provides potential benefits over STC's that include:

- Increased surface to volume ratio improving heat transfer
 - Enhanced radial mixing provided by oscillation
 - Reducing cost, space and production time
- Provides the ability to linearly scale up

The focus of this work is to:

- Improve understanding of nucleation and growth in a COBC
- Illustrate control of physically pure solids with desired particle size
- Develop a methodology for reliable continuous crystallisation

3. Continuous Crystallisations – Polymorphism and particle size distribution

Figure 3 shows the set-up used for continuous crystallisations. A below oscillates (Re_o 560-3100) the crystallising fluid while a peristaltic pump provides a net flow (Re_n 70-280) from the feeding vessel.

Process conditions applied in batch crystallisation allowing for polymorph selectivity where implemented in the COBC. Successful unseeded continuous crystallisation of pure α achieved.



Fig 3 COBC DN15 - working volume of 3.2L

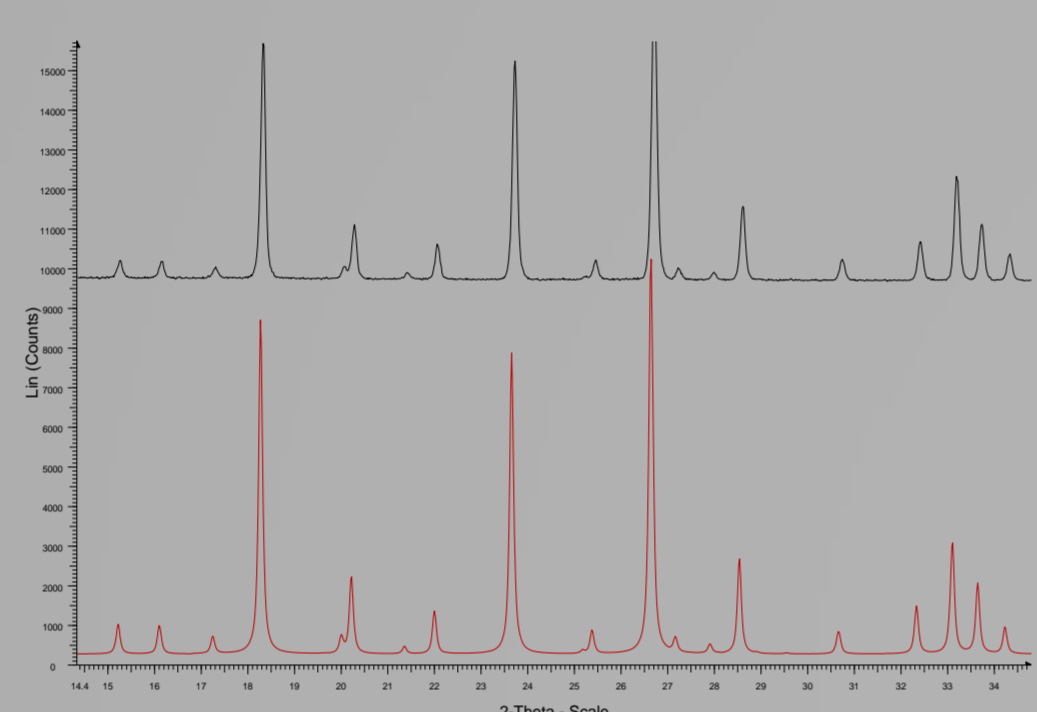


Fig 4 x-ray powder diffraction pattern of α generated from; single crystal data (red) and experimental crystallisation (black)

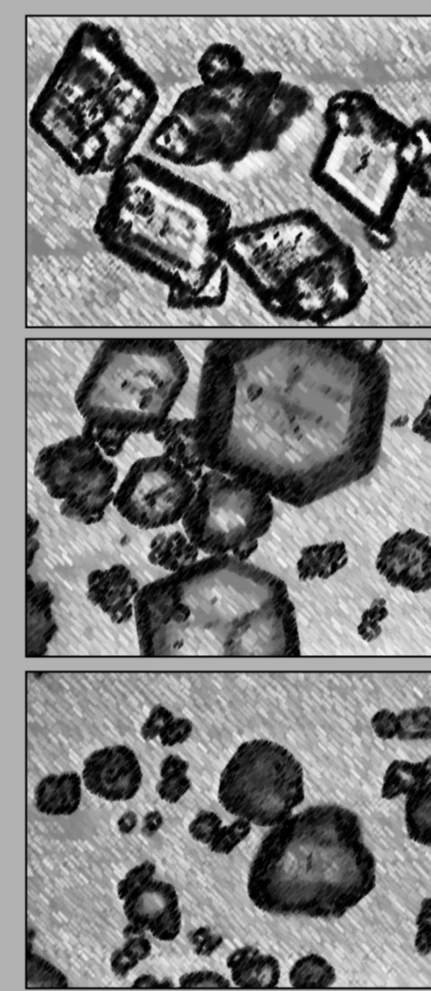


Fig 5 α from COBC

4. Process Optimisation – Steps to improve control over product attributes

1) Implementation of Process Analytical Technology (PAT) in COBC: Recent modification of COBC glass bends allow for in-situ monitoring of the crystallisation process in real time. The design allows probes to be removed and inserted at different positions along the COBC length providing quantitative information about solution concentration, nucleation and crystal size.

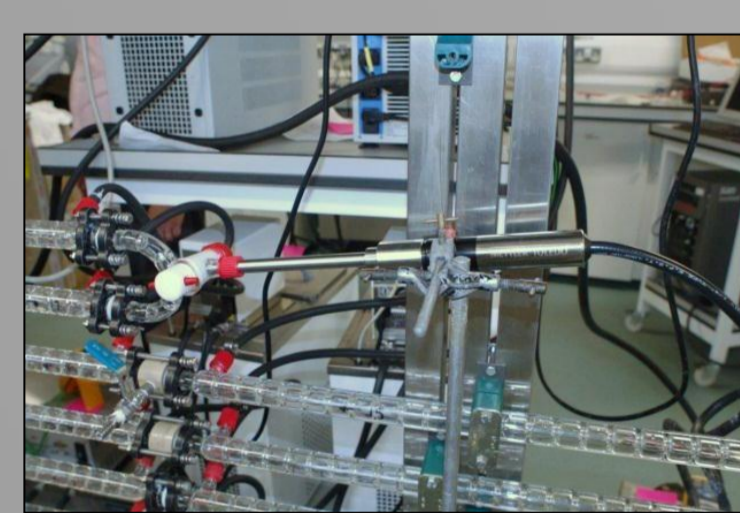


Fig 11 FBRM probe

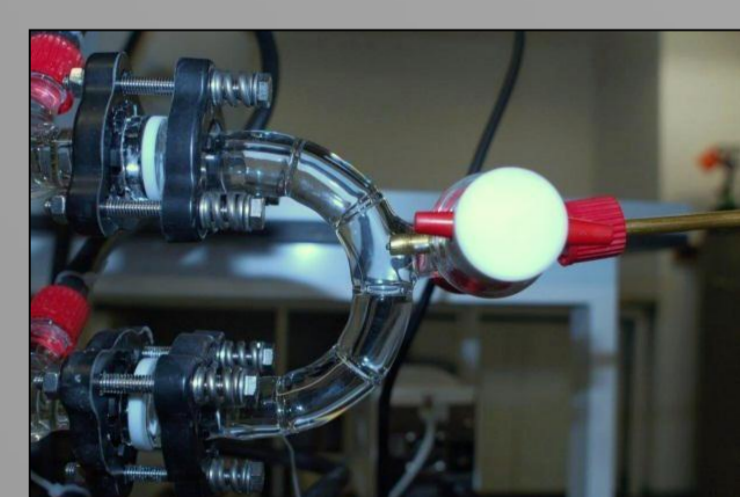


Fig 12 Mid-IR ATR probe

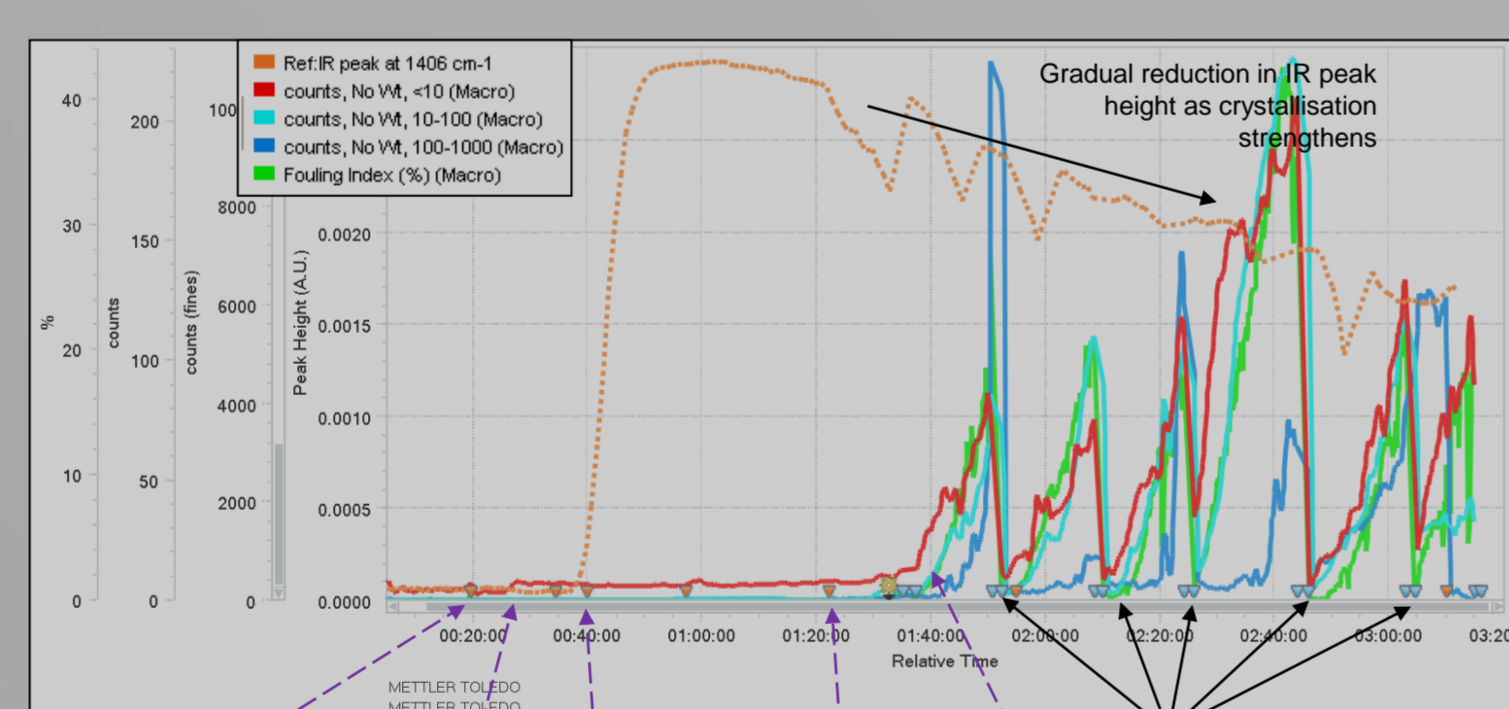
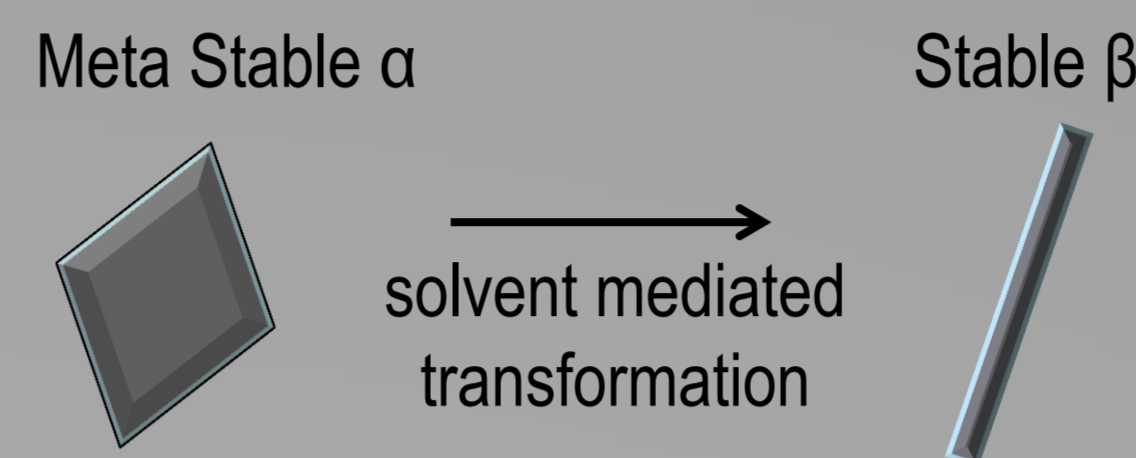


Fig 13 On-line monitoring during a continuous crystallisation

2. L-Glutamic Acid

Two known polymorphs of L-Glutamic acid (LGA):



Monotropic system where solvent mediated transformation rates are significantly increased at elevated temperatures.

Different forms can be readily identified using techniques such as X-ray diffraction and Raman spectroscopy.



Fig 1 Mettler Toledo Optimax system set up for solubility measurement

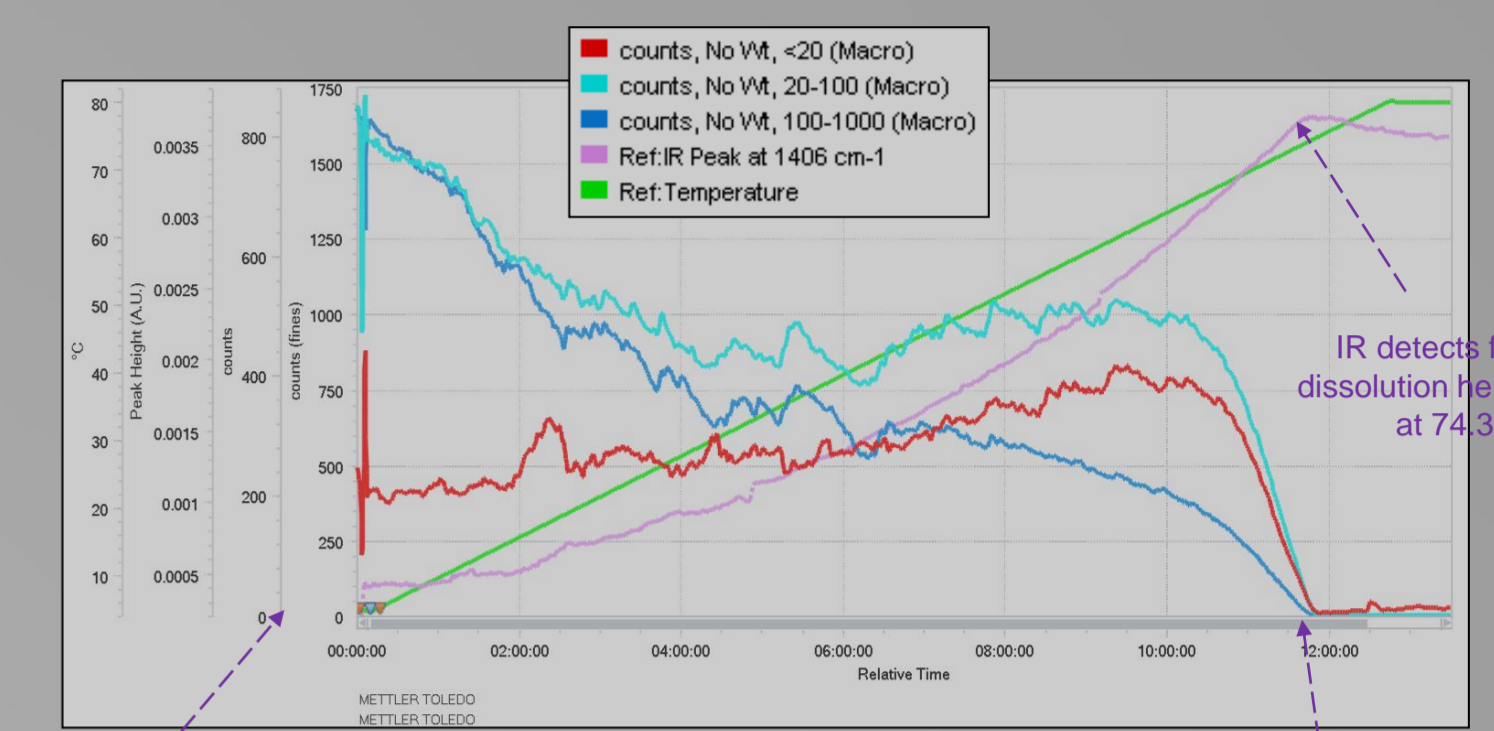


Fig 2 Solubility data

β Solubility measured using the "calibration-free" method with an FBRM and mid-IR probe in-situ.

Interestingly when implementing batch crystallisation conditions for the production of β , the stable form could not be isolated in pure phase.

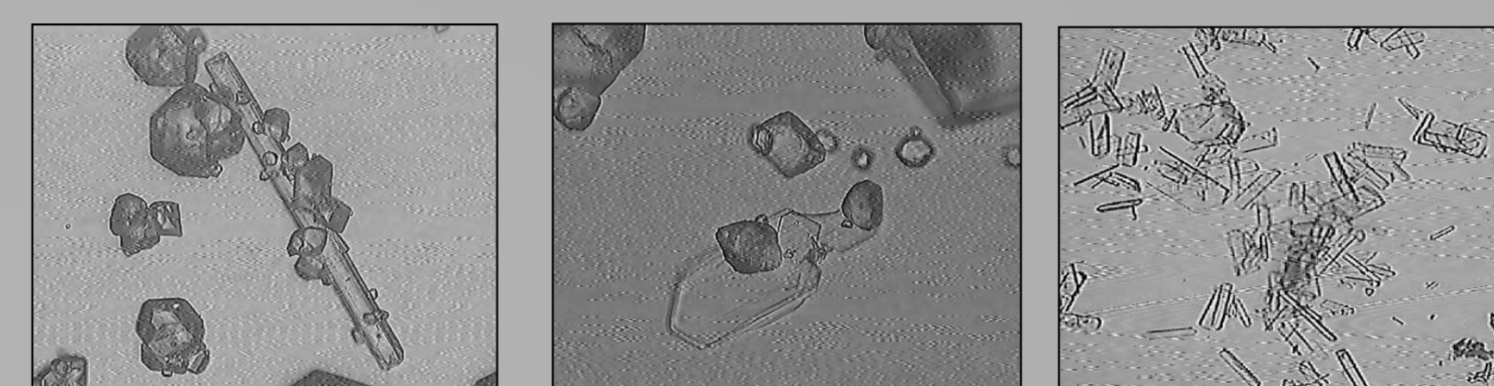


Fig 6 β co-existing with α

Fig 7 β co-existing with α

Fig 8 Pure phase β

Physically pure β LGA can be produced via a seeded continuous crystallisation process under conditions which, without seeding, result in a mixed phase product. Unaided production of pure β remains a challenge.

Evidence of fines in particle size distributions suggests secondary nucleation/attrition is occurring during crystallisation. Evidence of crystal breakage is observed with larger crystals (>800 μ m).

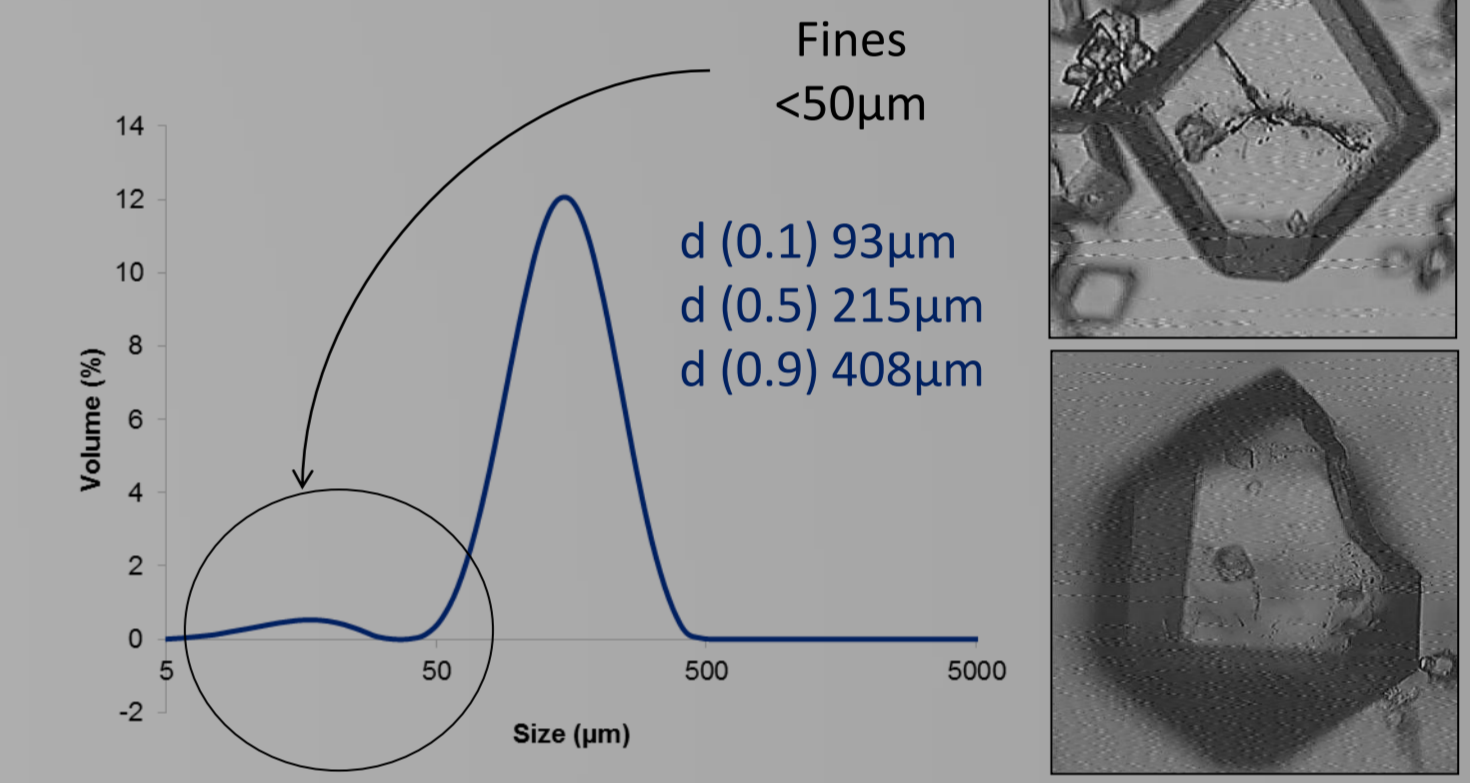


Fig 9 Malvern Mastersizer PSD data

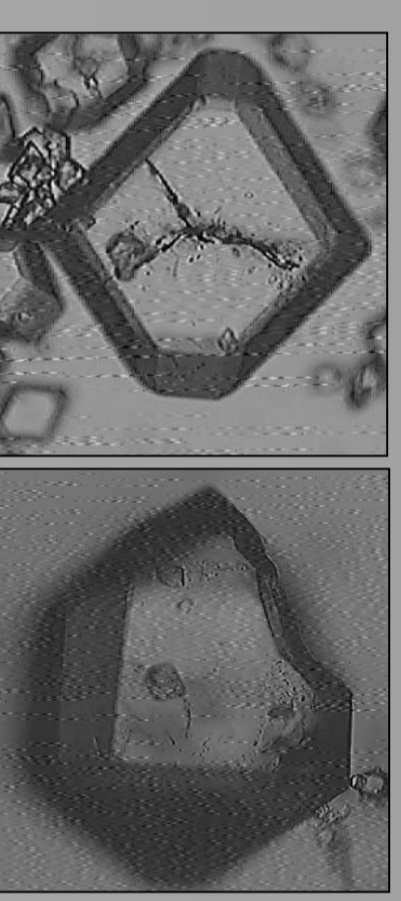


Fig 10 Observed crystal breakage

5. Further Work

Each of the following stages are required for development of reliable unseeded crystallisation processes of α and β LGA.

1) Better control over primary nucleation without excessive supersaturation

Pre-nucleated feed and utilisation of COBC as a growth unit. Use of ultra sonics of nucleation induction.

2) Use of PAT

Provides the opportunity for dynamic process control

3) Alternative solvent systems

Screening of water:solvent systems to investigate reduction of encrustation

4) Design space of COBC operating parameters

Completion of RTD experiments with solid loadings to ensure correct flow conditions are achieved during COBC operation

5) Batch-Continuous Crystallisations

Assess crystallisation performance with oscillating fluid (encrustation not observed with moving baffles)

6. Summary

- α LGA is readily obtained through unseeded crystallisation in the COBC
- Continuous crystallisation of pure β remains a challenge but can be achieved via seeding
- Preliminary experiments indicate seeding significantly reduces the tendency for encrustation (a main focus of this research is understanding/controlling nucleation therefore seeding is not investigated further)
- Successful design and implementation of probe ports for on-line monitoring provides a means for dynamic process control
- Preliminary RTD experiments indicate reasonable plug flow has been achieved in continuous experiments to date (neglecting impact of solids content)
- Encrustation remains a major barrier to process optimisation



Fig 20 Encrustation on COBC walls

7. Acknowledgements

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